

Homogeneous relaxation models &
methods
for
compressible three-phase flow & more
II: Future perspectives

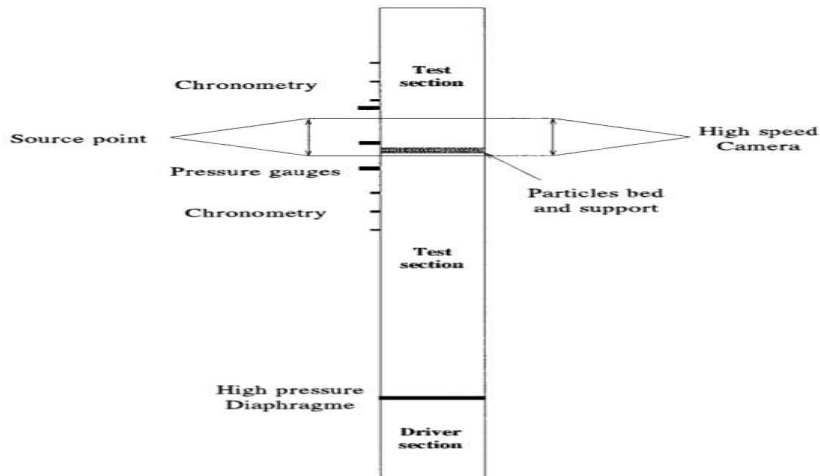
Keh-Ming Shyue

Institute of Applied Mathematical Sciences
National Taiwan University

May 8-12, 2017, CSRC, Beijing, China

Shock-induced particle fluidization: setup

Schematic experimental setup (taken from Rogue *et al.* (Shock wave 1998) & so plots in following 4 slides)



Particle fluidization: Drag coefficient measurement

Table 1. Summary of experimental results on drag coefficient

Gases Driver/Driven	Mach number	Particle diameter (mm)	Particle material	C_d	Reynolds range
Air/Air	1.291	2	Glass	0.61	27 000–30 000
Air/Air	1.298	2	Nylon	0.57	25 000–31 000
Air/Air	1.29	1	Glass	0.54	12 000–14 800
SF ₆ /SF ₆	1.341	2	Glass	0.62	80 000–119 000
SF ₆ /SF ₆	1.341	2	Nylon	0.62	79 000–116 000
SF ₆ /SF ₆	1.354	1	Glass	0.58	44 000–62 000
SF ₆ /Air	1.217	2	Nylon	0.51	17 000–21 000
SF ₆ /Air	1.218	1	Glass	0.50	7 200–10 000
Air/Helium	1.181	2	Nylon	0.57	5 000–6 000

Particle fluidization: Collective particle behavior

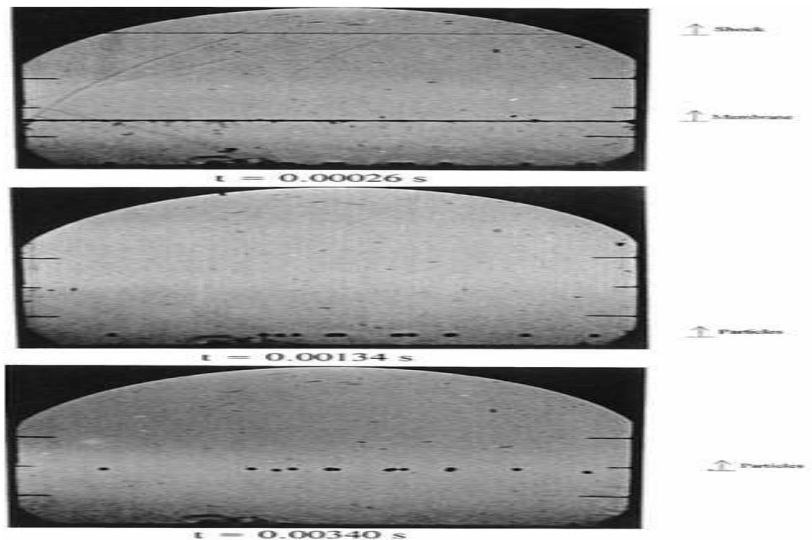


Fig. 7. A few 2 mm diameter nylon particles on a plastic membrane, shock Mach= 1.3 in air

Particle fluidization: Collective particle behavior

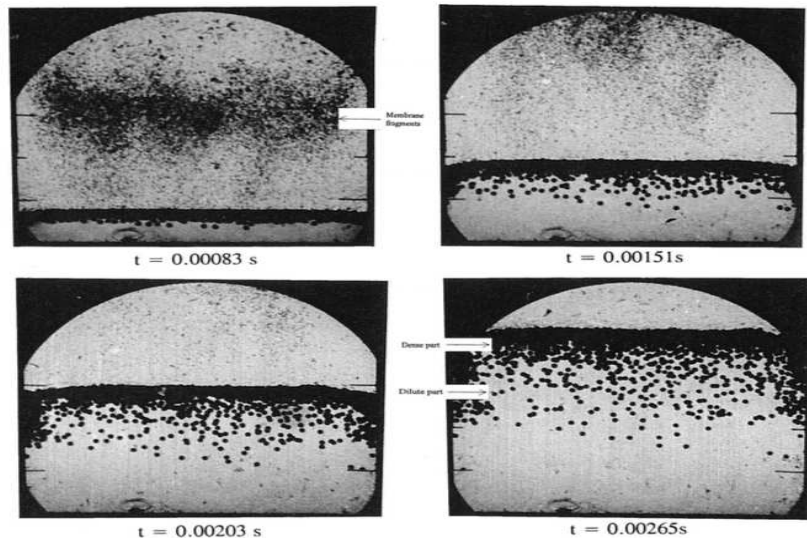
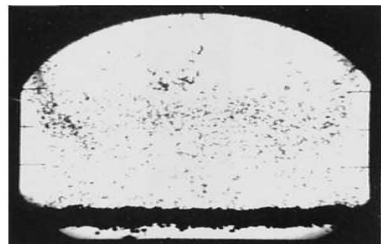
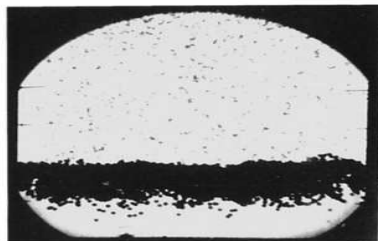


Fig. 9. A single layer of 2 mm diameter glass particles on a plastic membrane, Shock Mach=1.3 in air

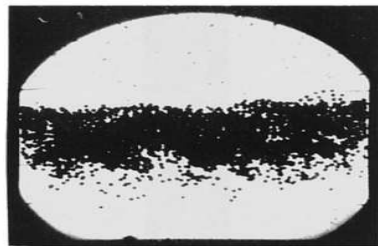
Particle fluidization: Collective particle behavior



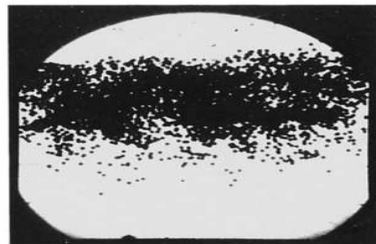
$t = 0.00150 \text{ s}$



$t = 0.00228 \text{ s}$



$t = 0.00318 \text{ s}$



$t = 0.00384 \text{ s}$

Fig. 11. A double layer of 2 mm diameter glass particles on a plastic membrane, Shock Mach=1.3 in air

Particle fluidization: Collective particle behavior

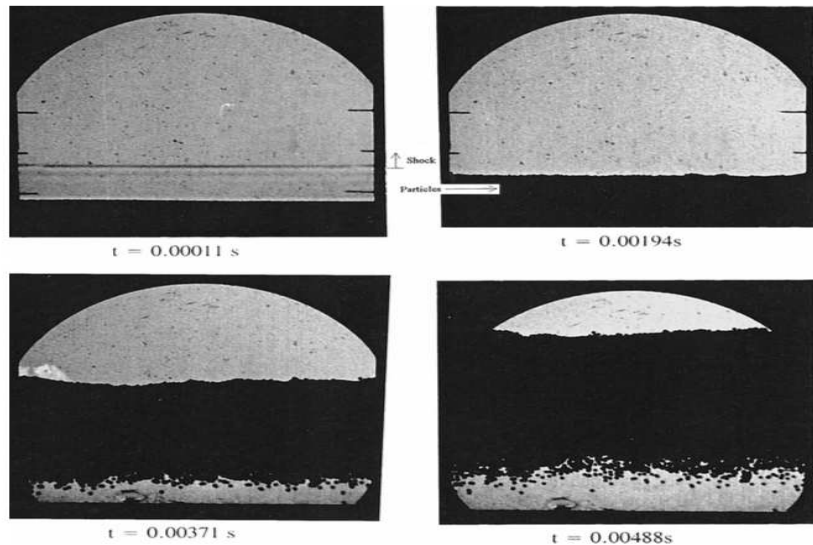
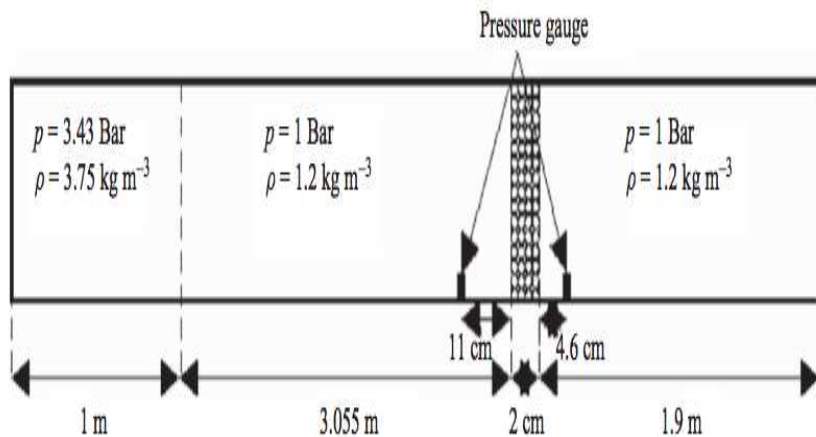


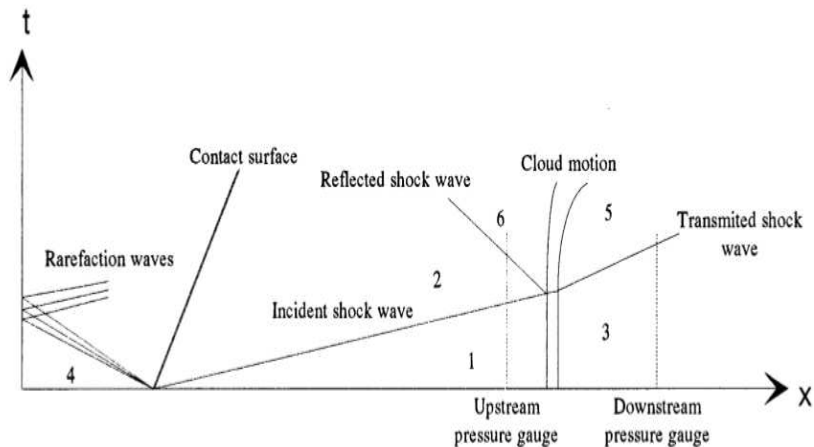
Fig. 13. A 2 cm thick bed of 1.5 mm diameter glass particles on a metal grid, shock Mach=1.3 in air

Particle fluidization: numerical setup



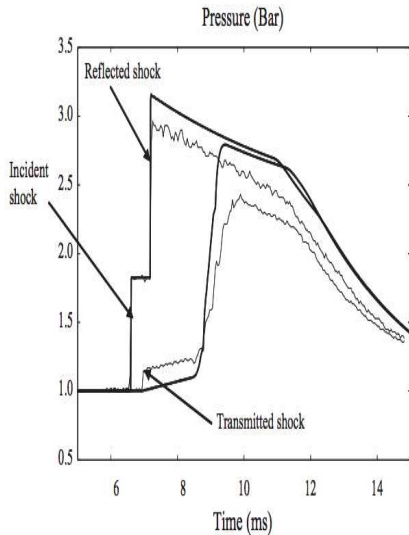
Particle fluidization: Wave pattern

Schematic $x-t$ diagram of two-phase flow in shock tube

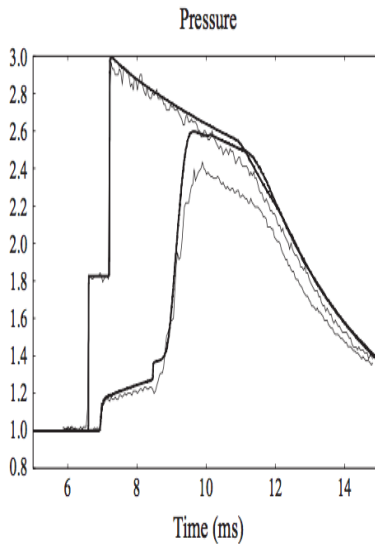


Particle fluidization: Diagnosis

without drift velocity

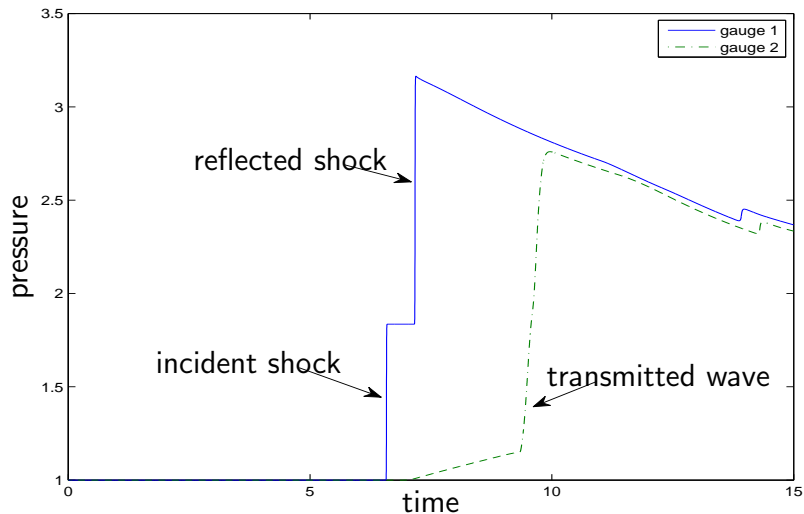


with drift velocity



Particle fluidization: Diagnosis

Results obtained using 5-equation transport model



Particle fluidization: 6-equation model

Saurel *et al.* (JFM 2010) proposed compressible 2-phase (fluid-solid (granular material)) model as

$$\partial_t (\alpha_1 \rho_1) + \nabla \cdot (\alpha_1 \rho_1 \vec{u}) = 0$$

$$\partial_t (\alpha_2 \rho_2) + \nabla \cdot (\alpha_2 \rho_2 \vec{u}) = 0$$

$$\partial_t (\rho \vec{u}) + \nabla \cdot (\rho \vec{u} \otimes \vec{u}) + \nabla p = 0$$

$$\partial_t ((\alpha \rho)_1 (e + B)_1) + \nabla \cdot ((\alpha \rho)_1 (e + B)_1 \vec{u}) + (\alpha p)_1 \nabla \cdot \vec{u} = \mu \pi_I (\pi_2 - \pi_1)$$

$$\partial_t ((\alpha \rho)_2 (e + B)_2) + \nabla \cdot ((\alpha \rho)_2 (e + B)_2 \vec{u}) + (\alpha p)_2 \nabla \cdot \vec{u} = -\mu \pi_I (\pi_2 - \pi_1)$$

$$\partial_t (\rho E) + \nabla \cdot (\rho E \vec{u} + p \vec{u}) = 0$$

$$\partial_t \alpha_1 + \vec{u} \cdot \nabla \alpha_1 = \mu (\pi_1 - \pi_2)$$

π_k : phasic total stress, β_k : granular pressure, & B_k granular energy; $k = 1$ solid phase & $k = 2$ fluid phase

In addition, for $k = 1, 2$, we have

$$\pi_k = p_k - \beta_k$$

$$\pi_I = (\rho_2 c_2 \pi_1 + \rho_1 c_1 \pi_2) / (\rho_1 c_1 + \rho_2 c_2)$$

$$E_k = e_k + B_k + \frac{1}{2} \vec{u} \cdot \vec{u}$$

$$E = Y_1 E_1 + Y_2 E_2$$

$$p = \alpha_1 p_1 + \alpha_2 p_2$$

Relaxation parameter μ assumed to satisfy

$$\mu = \begin{cases} \infty & \text{if } \pi_1 > \pi_2, \\ 0 & \text{otherwise,} \end{cases}$$

Constitutive laws

1. Equation of state for fluid (stiffened gas EOS)

$$p_k = (\gamma_k - 1)\rho_k e_k - \gamma_k p_{\infty, k}$$

2. Granular energy of the form

$$B_k(\alpha) = \begin{cases} B_a(\alpha) & \text{if } \alpha_0 < \alpha < 1, \\ 0 & \text{otherwise,} \end{cases}$$

$$B_a(\alpha) = a [(1 - \alpha) \log(1 - \alpha) + (1 + \log(1 - \alpha_0))(\alpha - \alpha_0) - (1 - \alpha_0) \log(1 - \alpha_0)]^n$$

3. Granular pressure

$$\beta_k = (\alpha\rho)_k \frac{dB_k}{d\alpha_k}$$

Parameters a , n , & α_0 are material-dependent quantities for given powder

7-equation model

Baer-Nunziato (Intl. J. Multiphase Flows 1986)

$$\partial_t (\alpha_1 \rho_1) + \nabla \cdot (\alpha_1 \rho_1 \vec{u}_1) = 0$$

$$\partial_t (\alpha_2 \rho_2) + \nabla \cdot (\alpha_2 \rho_2 \vec{u}_2) = 0$$

$$\partial_t (\alpha_1 \rho_1 \vec{u}_1) + \nabla \cdot (\alpha_1 \rho_1 \vec{u}_1 \otimes \vec{u}_1) + \nabla (\alpha_1 p_1) = \pi_I \nabla \alpha_1 - \lambda \vec{u}_R$$

$$\partial_t (\alpha_2 \rho_2 \vec{u}_2) + \nabla \cdot (\alpha_2 \rho_2 \vec{u}_2 \otimes \vec{u}_2) + \nabla (\alpha_2 p_2) = -\pi_I \nabla \alpha_1 + \lambda \vec{u}_R$$

$$\begin{aligned} \partial_t (\alpha_1 \rho_1 E_1) + \nabla \cdot (\alpha_1 \rho_1 E_1 \vec{u}_1 + \alpha_1 p_1 \vec{u}_1) = \\ \pi_I \vec{u}_I \nabla \alpha_1 - \lambda \vec{u}'_I \vec{u}_R - \mu \pi_I \pi_R \end{aligned}$$

$$\begin{aligned} \partial_t (\alpha_2 \rho_2 E_2) + \nabla \cdot (\alpha_2 \rho_2 E_2 \vec{u}_2 + \alpha_2 p_2 \vec{u}_2) = \\ -\pi_I \vec{u}_I \nabla \alpha_1 + \lambda \vec{u}'_I \vec{u}_R + \mu \pi_I \pi_R \end{aligned}$$

$$\partial_t \alpha_1 + \vec{u} \cdot \nabla \alpha_1 = \mu \pi_R$$

$$\pi_R = \pi_1 - \pi_2 \quad \& \quad \vec{u}_R = \vec{u}_1 - \vec{u}_2$$

μ & λ : Relaxation parameters

5-equation model with drift effects

Saurel *et al.* (JFM 2010)

$$\partial_t (\alpha_1 \rho_1) + \nabla \cdot (\alpha_1 \rho_1 \vec{u}) + \nabla \cdot (\rho Y_1 Y_2 \vec{u}_R) = 0$$

$$\partial_t (\alpha_2 \rho_2) + \nabla \cdot (\alpha_2 \rho_2 \vec{u}) - \nabla \cdot (\rho Y_1 Y_2 \vec{u}_R) = 0$$

$$\partial_t (\rho \vec{u}) + \nabla \cdot (\rho \vec{u} \otimes \vec{u}) + \nabla p = 0$$

$$\begin{aligned} \partial_t (\rho E) + \nabla \cdot (\rho E \vec{u} + p \vec{u}) + \\ \nabla \cdot (\rho Y_1 Y_2 \vec{u}_R ((h + B)_1 - (h + B)_2)) = 0 \end{aligned}$$

$$\partial_t \alpha_1 + \vec{u} \cdot \nabla \alpha_1 =$$

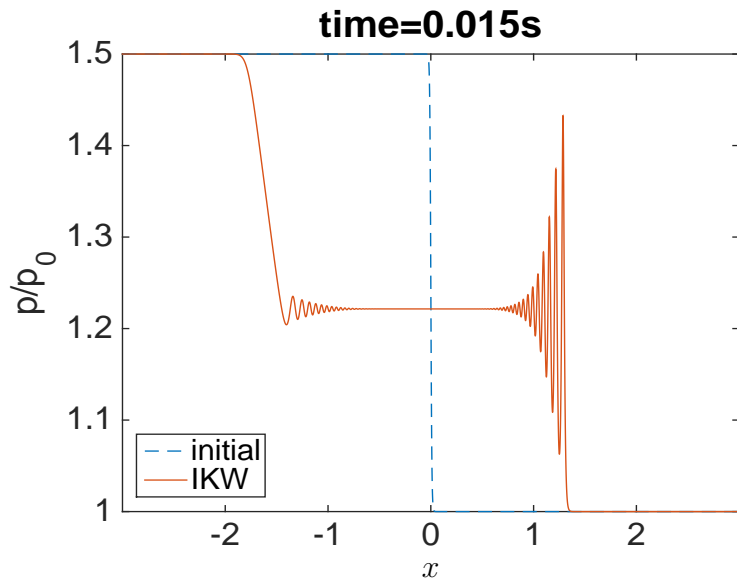
$$\begin{aligned} \rho c_w^2 \frac{\alpha_1 \alpha_2}{\rho_1 c_1^2 \rho_2 c_2^2} \left[((\rho_2 c_2^2 - \beta_2) - (\rho_1 c_1^2 - \beta_1)) \nabla \cdot \vec{u} - \right. \\ \left. \left(\frac{\rho_1 c_1^2 - \beta_1}{\alpha_1 \rho_1} + \frac{\rho_2 c_2^2 - \beta_2}{\alpha_2 \rho_2} \right) \nabla \cdot (\rho Y_1 Y_2 \vec{u}_R) - \right. \\ \left. \rho Y_1 Y_2 \vec{u}_R \cdot \left(\frac{\Gamma_1}{\alpha_1} T_1 \nabla s_1 + \frac{\Gamma_2}{\alpha_2} T_2 \nabla s_2 \right) \right] \end{aligned}$$

$u_R \approx \vec{u}_1 - \vec{u}_2$ takes form

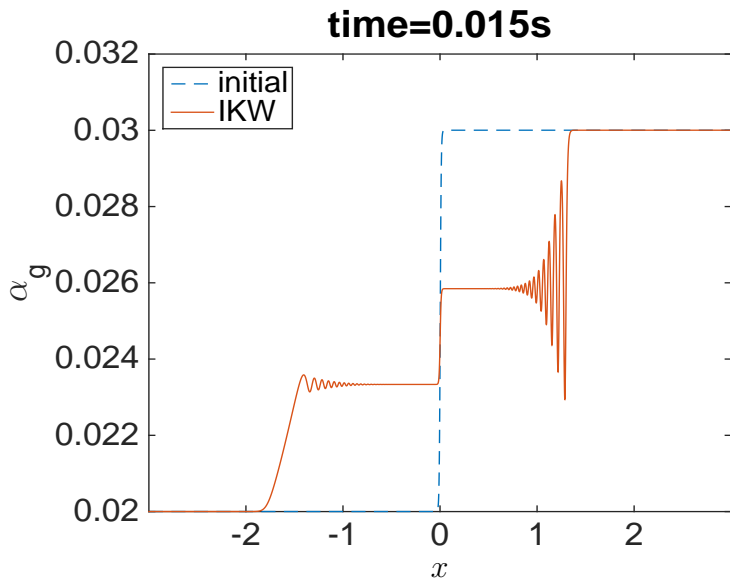
$$\vec{u}_R = \frac{1}{\lambda} ((\alpha_1 - Y_1) \nabla p - \alpha_2 \nabla (\alpha_1 \beta_1) + \alpha_1 \nabla (\alpha_2 \beta_2))$$

There exists 6-equation model with drift effects (not given here)

Riemann problem: IKW model



Riemann problem: IKW model



Bubbly flow in liquid

lordanski-Kogarko-Wijngaarden model for bubbly flow in liquid takes form

$$\partial_t \rho + \nabla \cdot (\rho \vec{u}) = 0$$

$$\partial_t (\rho \vec{u}) + \nabla \cdot (\rho \vec{u} \otimes \vec{u}) + \nabla p = 0$$

$$\partial_t (\alpha_g \rho_g) + \nabla \cdot (\alpha_g \rho_g \vec{u}) = 0$$

$$\partial_t N_b + \nabla \cdot (N_b \vec{u}) = 0$$

To close the model, assumptions are:

1. The liquid phase is assumed to be incompressible, where ρ_l is set to be a chosen constant.
2. The volume fraction of the gas α_g is assumed to satisfy the relation

$$\alpha_g = \frac{4}{3} \pi R^3 N_b,$$

where R is the bubble radius.

3. The gas inside the bubble is assumed to be ideal & takes

$$p_g = p_0 \left(\frac{R_0}{R} \right)^{3\gamma},$$

4. Assume mixture pressure p follow Rayleigh-Plesset equation

$$p = p_g(R) - \rho_l \left(R\ddot{R} + \frac{3}{2}\dot{R}^2 \right) - 4\mu_l \frac{\dot{R}}{R}.$$

Here μ_l is the dynamic viscosity of the liquid, and \dot{R} means dR/dt .

5. Bubble distribution is assumed to be uniform, *i.e.*, the flow is in the absence of bubble breakup and coalescence

Impact-shear 2-phase Riemann problem

Table: Material-dependent quantities used in the stiffened gas equation of state for the simulation

	γ	p_∞ (GPa)	μ (GPa)	ρ_0 (kg/m ³)
Titanium	2.6	44	42	4527
Aluminum	3.5	3.2	26	2712

Initial condition:

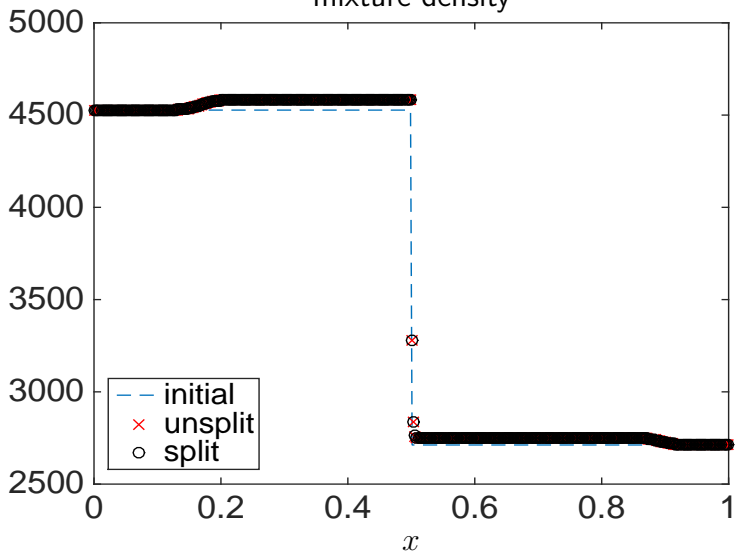
- Titanium phase: Left-hand side ($0 \leq x \leq 0.5\text{m}$)

$$(\rho_1, \rho_2, u, v, p, \alpha_1)_L = (4527, 2712, 10^2, 10^2, 10^5, 1 - 10^{-8})$$

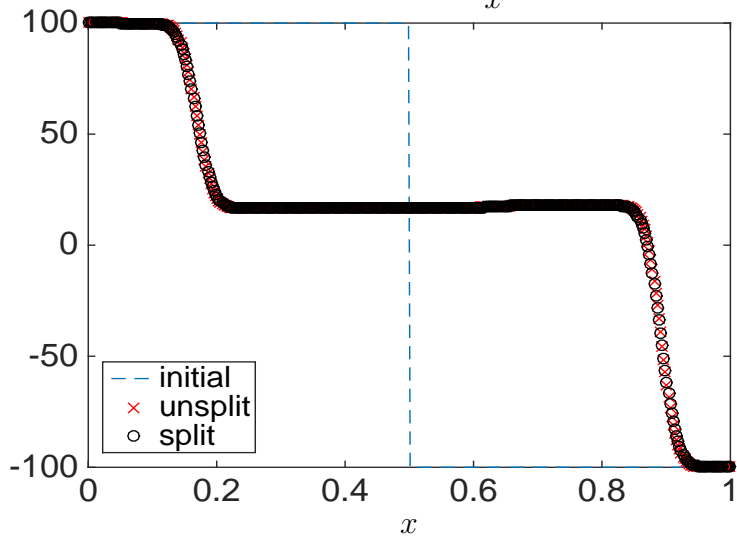
- Aluminum phase: Right-hand side ($0.5\text{m} < x \leq 1\text{m}$)

$$(\rho_1, \rho_2, u, v, p, \alpha_1)_L = (4527, 2712, -10^2, -10^2, 10^5, 10^{-8})$$

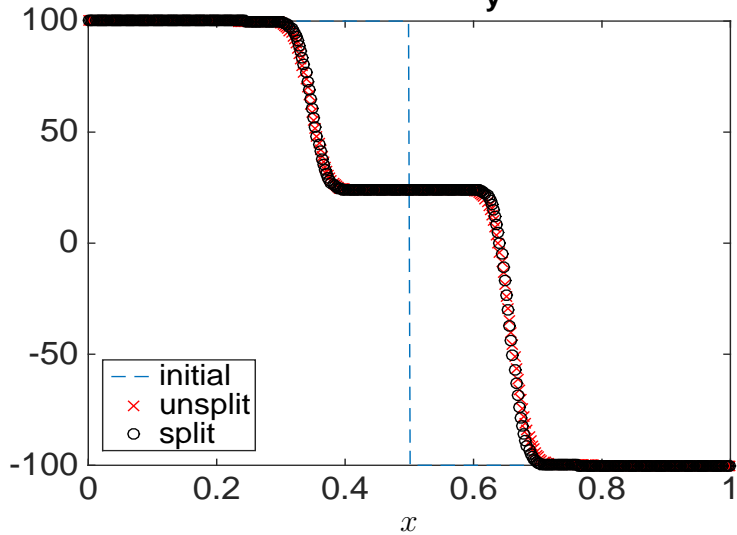
mixture density

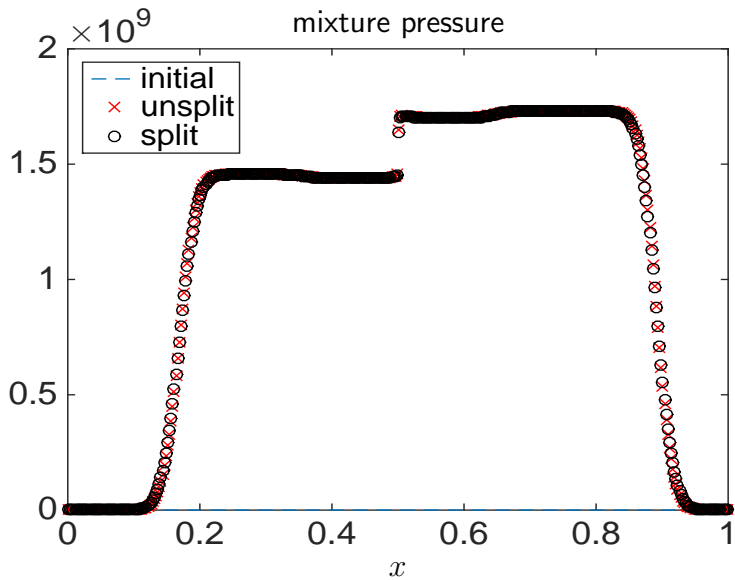


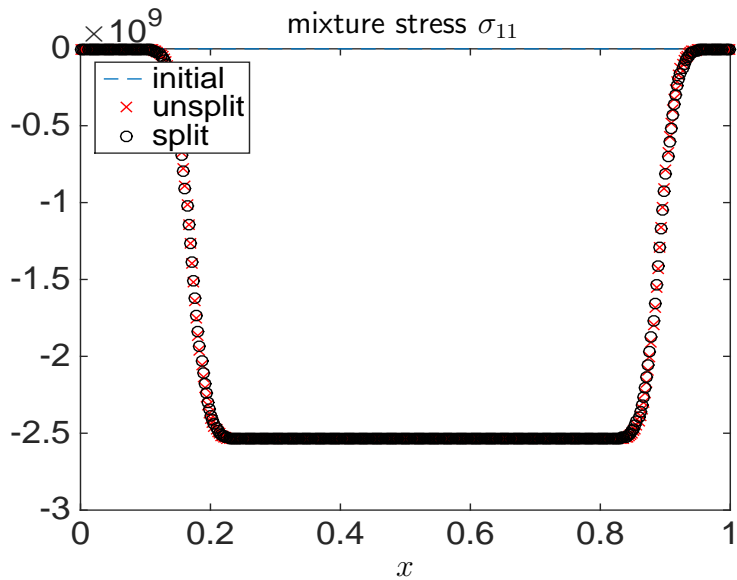
velocity v_x

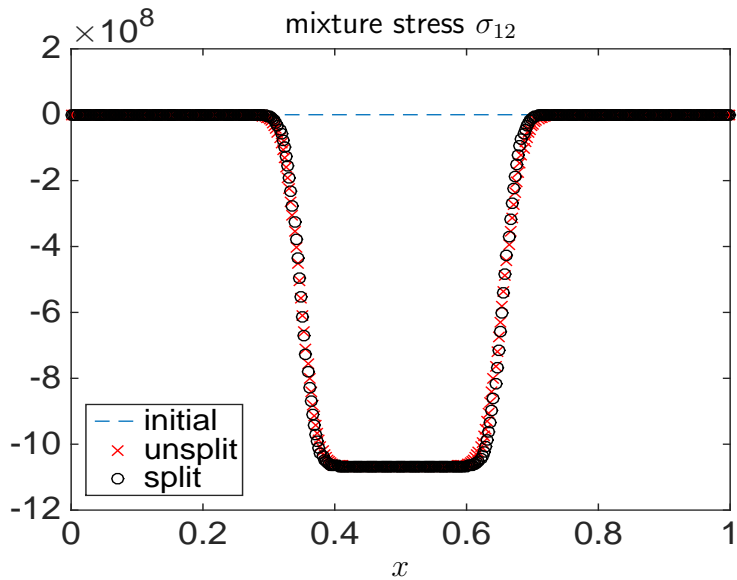


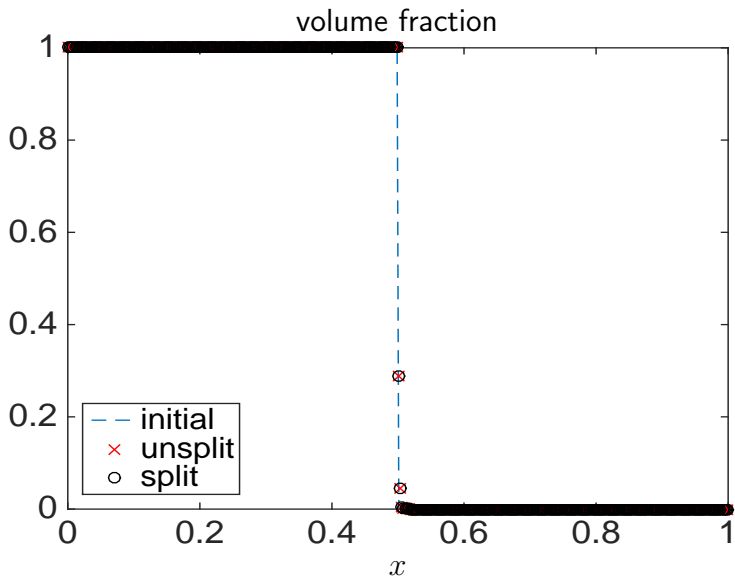
velocity v_y











Model for hyperelastic flow

Ndanou *et al.* (JCP 2015) proposed

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho u) = 0$$

$$\frac{\partial}{\partial t} (\rho u) + \nabla \cdot (\rho u \otimes u - \sigma) = 0$$

$$\frac{\partial E}{\partial t} + \nabla \cdot (Eu - \sigma u) = 0$$

$$\frac{\partial e^\beta}{\partial t} + \nabla (u \cdot e^\beta) = 0$$

$$\nabla \times e^\beta = 0$$

Consider internal energy e_k for each phase in separable form

$$e_k = e_k^h(\rho_k, p_k) + e_k^e(g_k)$$

Assume hydrodynamic energy e_k^h follows stiffened gas EOS as

$$e_k^h(\rho_k, p_k) = \frac{p_k + \gamma_k p_{\infty k}}{\gamma_k - 1}$$

For isotropic solids, elastic energy e_k^e assumes

$$e_k^e(g_k) = e_k^e(j_{1k}, j_{2k})$$

$$j_{1k} = \text{trace}(g_k)$$

$$j_{2k} = \text{trace}(g_k^2)$$

For applications, we take

$$e_k^e(g_k) = \frac{\mu_k}{8\rho_{0k}} (j_{2k} - 3)$$

or

$$e_k^e(g_k) = \frac{\mu_k}{4\rho_{0k}} \left(\theta j_{2k} + \frac{1 - 2\theta}{3} j_{1k}^2 + 3(\theta - 1) \right)$$

$$g_k = \frac{G_k}{|G_k|^{1/3}}, \quad |G_k| = \det(G_k)$$

Let $X_k = \{X_k^i\}$ be Lagrangian coordinates for solid k

Denote e_k^i as being local cobasis of form

$$e_k^i = \nabla_x X_k^i = (a_k^i, b_k^i, c_k^i)$$

Define deformation gradient F_k as

$$F_k^{-T} = (e_k^1, e_k^2, e_k^3)$$

Then Finger tensor G_k takes form

$$G_k = F_k^{-T} F_k^{-1} = \sum_{i=1}^3 e_k^i \otimes e_k^i$$

Denote σ to be total stress as

$$\sigma = \sum_k \alpha_k \sigma_k$$

with phasic stress tensor σ_k defined by

$$\sigma_k = -2\rho_k \frac{\partial e_k}{\partial G_k} G_k = -p_k I + S_k$$

$$p_k = \rho_k^2 \frac{\partial e_k^h}{\partial \rho_k}$$

$$\begin{aligned} S_k &= -2\rho_k \frac{\partial e_k^e}{\partial G_k} G_k \\ &= -2\rho_k \left[2 \frac{\partial e_k^e}{\partial j_{2k}} \left(g_k^2 - \frac{j_{2k}}{3} I \right) + \frac{\partial e_k^e}{\partial j_{1k}} \left(g_k - \frac{j_{1k}}{3} I \right) \right] \end{aligned}$$

Model is hyperbolic with sound speed $c \in \mathbf{R}$ defined by

$$c_k^2 = \frac{\partial p}{\partial \rho} - \frac{\partial S_{11}}{\partial \rho} - \frac{1}{\rho} \left(\frac{\partial S_{11}}{\partial a} \cdot a \right) \\ - \frac{\partial S_{11}}{\partial \rho} - \frac{1}{\rho} \left(\frac{\partial S_{11}}{\partial a} \cdot a \right) = \frac{\partial e^e}{\partial a} \cdot a + \frac{\partial}{\partial a} \left(\frac{\partial e^e}{\partial a} \cdot a \right) \cdot a$$

Lecture summary

- Fluid-mixture type models & methods for compressible multicomponent flow
 1. Linear equation of state
 2. Nonlinear equation of state
- Homogeneous relaxation models & methods for compressible two-phase flow
 3. Reduced models
 4. Nonlinear equation of state
- Homogeneous relaxation models & methods for compressible three-phase flow & more
 5. Reduced 4-equation based models
 6. Future perspectives

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All lecture slides are available at CSRC course website:

<http://www.csrc.ac.cn/en/event/schools/2017-03-31/25.html>

Thank you